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DMF Recovery and Distillation System - 588 lbs/Hr

Capacity: 588 lbs/hour

Products: Dimethylformamide

Major Equipment

- Feed Preheater (HE-7001, 50 sq ft 316L SS shell and tube heat exchanger)
- Steam Heater (HE-7002, 9 sq ft 316L SS shell and tube heat exchanger)
- Distillation Column (CL-7001, 36" Dia, 40 trays, 59'3" tall)
- Bottoms Pump (PU-7002, 7.5 HP Hastelloy pump)
- Reboiler (HE-7003, 832 sg ft Hastelloy C276 shell and tube heat exchanger)
- Bottom Purge Cooler (HE-7006, 19 sq ft Hastelloy C276 shell and tube heat exchanger)
- 3-stage dual cartridge filters
- Bottoms Pump (PU-7002, 7.5 HP Hastelloy pump)
- Feed Preheater (HE-7001, 50 sq ft 316L SS shell and tube heat exchanger)
- Product Cooler (HE-7004, 50 sq ft 316L SS shell and tube heat exchanger)
- Column Condenser (HE-7005, 305 sq ft heat exchanger)
- Reflux Drum (TK-7002, 150-gallon SS tank)
- Reflux Pump (PU-7004, 2 HP pump)
- Heat Recovery Condenser (HE-7007, 305 sq ft

Brief Plant Description

The used skid-mounted DMF (Dimethylformamide) distillation system, designed by KOCH, recovers 14-35% DMF from wastewater. It includes a Distillation Column (CL-7001) with Koch-Glitsch valve trays, as well as several heat exchangers: Feed Preheater (HE-7001), Steam Heater (HE-7002), Reboiler (HE-7003), Product Cooler (HE-7004), Column Condenser (HE-7005), Bottom Purge Cooler (HE-7006), and Heat Recovery Condenser (HE-7007), plus the Reflux Drum (TK-7002) and pumps PU-7002, PU-7003, and PU-7004. Steam, cooling water, electricity, and instrument air power the system.

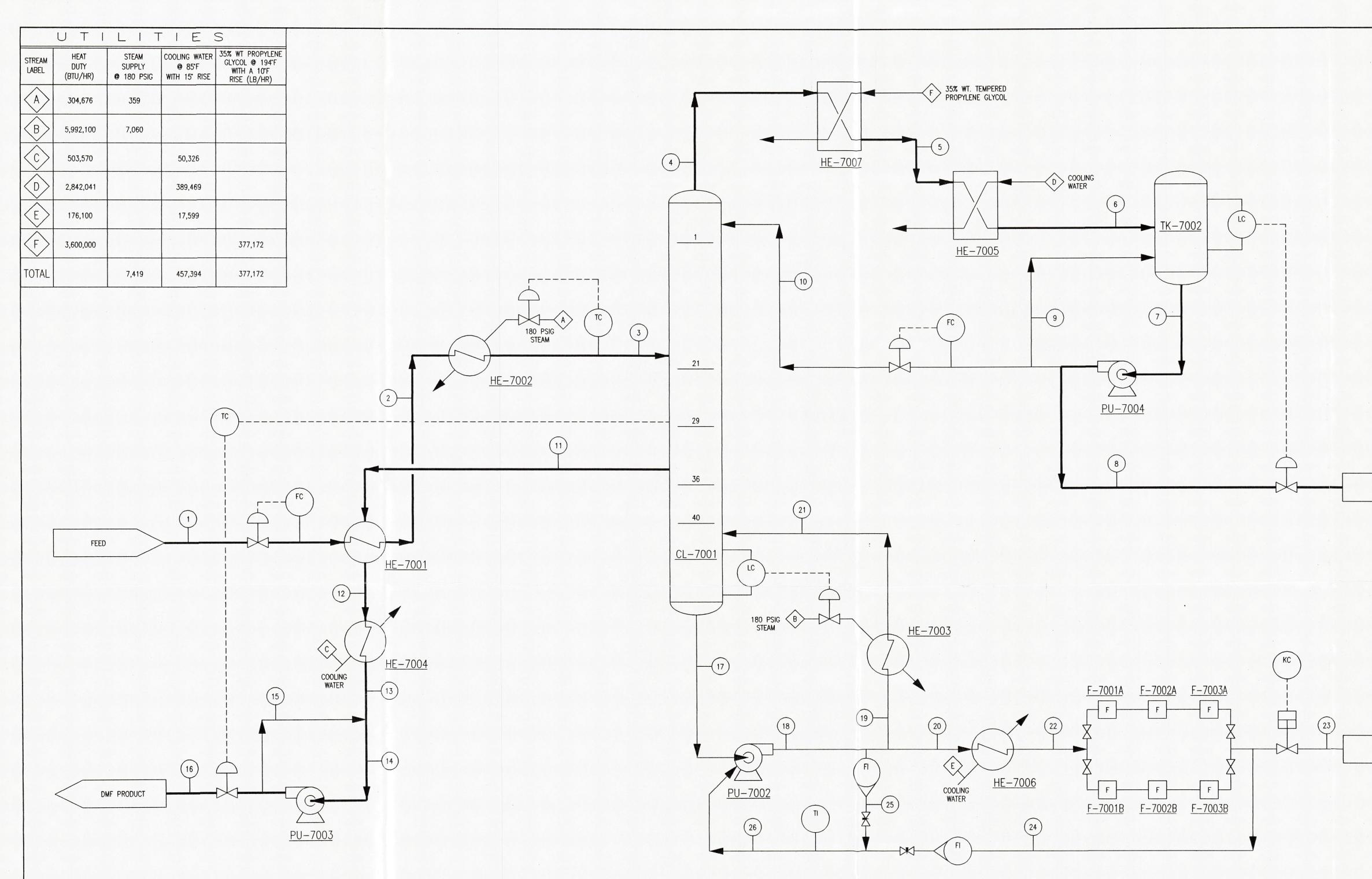
Wastewater containing DMF, water, and formic acid is fed into the system via the Feed Preheater and Steam Heater into the Distillation Column, operating at atmospheric pressure. The bottoms circulate through the Reboiler, where steam at 180 psig strips water from the feed. A formic acid-DMF azeotrope is removed via a small purge stream, cooled to 115°F, and filtered before partial recycling.

A vapor draw containing dry DMF is condensed and cooled to 115°F in the Product Cooler. Remaining vapor, containing steam and trace DMF, is condensed and subcooled in the Column Condenser. Condensate flows to the Reflux Drum, where it is either returned to the column as reflux or disposed of. When the Heat Recovery Condenser is used, vapors are partially condensed before final cooling. The DMF product contains less than 150 ppm water, with a distillate containing less than 0.1% DMF by weight.

For more

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MATERIAL STREAM NUMBE	BALAN R & IDEN		COLD FEED TO FEED PREHEATER HE-7001	WARM FEED TO STREAM HEATER HE-7002	HOT FEED COLUMN CL-7001	CL-7001 OVERHEAD VAPORS	FEED TO HE-7005 (NOTE 3)	CONDENSED OVERHEAD VAPORS TO TK-7002	CONDENSED OVERHEAD VAPORS TO PU-7004	DISTILLATE PRODUCT TO SEWER	MIN. FLOW RECYCLE FOR PUMP PU-7004	REFLUX TO COLUMN CL-7001	DMF VAPOR SIDE DRAW TO HE-7001	Condensed DMF TO PRODUCT COOLER HE-7004	COOLED DMF FROM PRODUCT COOLER HE-7004	DMF PRODUCT TO PRODUCT PUMP PU-7003	MIN. FLOW RECYCLE FOR PUMP PU-7003	DMF PRODUCT TO STORAGE	Column Bottoms To Pump PU-7002	Column Bottoms From Pump PU-7002	COLUMN BOTTOMS TO REBOILER HE-7003	PURGE STREAM TO HE-7006	REBOILER RETURN TO COLUMN CL-7001	Cooled Purge Stream to Filters	COOLED BOTTOMS PURGE TO TREATMENT (BY OTHERS)	Cold/filtered Bottoms Liquid Recycle
COMPONENT		MOL. WT.																								
1 WATER		18.015	3369.7	3369.7	3369.7	5487.2	5487.2	5487.2	5487.2	3369.6	3369.6	2117.5	0.1	0.1	0.1	0.1	0.1	0.1	0.9	1.0	0.9	0.0	0.9	0.0	0.00	0.0
2 DIMETHYLFORMAMIDE		73.095	594.7	594.7	594.7	5.5	5.5	5.5	5.5	3.4	3.4	2.1	588.1	588.1	588.1	588.1	469.1	588.1	110616.5	114027.2	110613.4	1517.6	110613.4	1517.6	3.16	1514.4
3 FORMIC ACID		46.026	0.2	0.2	0.2	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.2	0.2	0.2	0.2	0.1	0.2	1487.7	1533.6	1487.7	20.4	1487.7	20.4	0.04	20.4
4 SOLIDS		-	4.0	4.0	4.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	0.0	1147.9	1167.3	1132.3	15.5	1132.3	15.5	0.00	0.0
TOTAL	LB/HR		3969	3969	3969	5493	5493	5493	7950	3373.0	2457.6	2119.7	588.4	588.4	588.4	2907.8	2319.4	588.4	113253.1	116729.1	113234.3	1553.5	113234.3	1553.5	3.2	1534.8
TEMPERATURE	•F		70	121	200	218	218	140	140	140	140	140	328	200	115	115	115	115	330	328	328	328	330	115	115	115
PRESSURE	PSIG		40	15.7	3.5	2.0	1.0	0.3	22.5	20.0	43.8	2.0	4.8	4.5	10.0	10.0	35.0	15.0	8.6	26.5	6.0	26.5	4.9	25.0	5.0	20.0
DENSITY	LB/FT 3		61.755	60.967	59.319	0.04011	59.685	61.522	61.522	61.281	61.281	61.281	0.176	54.843	57.703	57.703	57.703	57.703	51.534	51.546	51.546	51.546	0.174	57.9	57.703	57.703
VISCOSITY	сР		0.970	0.553	0.304	0.012	0.275	0.474	0.474	0.463	0.463	0.463	0.010	0.394	0.634	0.634	0.634	0.634	0.249	0.249	0.249	0.249	0.011	0.634	0.634	0.634
FLOW	GPM(ACFM)		8.0	8.1	8.3	(2282)	11.5	11.1	16.1	6.9	5.0	4.3	(55.8)	1.3	1.3	6.3	5.0	1.3	274.0	282.3	273.9	3.8	(10846)	3.3	0.01	3.3
HEAT CAPACITY	BTU/LB'F		0.922	0.924	0.934	0.500	1.002	1.000	1.000	0.998	0.998	0.998	0.412	0.526	0.503	0.503	0.503	0.503	0.575	0.575	0.575	0.575	0.413	0.503	0.503	0.503
THERMAL COND.	BTU/HR'F.FT		0.261	0.252	0.347	0.014	0.393	0.371	0.371	0.373	0.373	0.373	0.011	0.091	0.101	0.101	0.101	0.101	0.081	0.081	0.081	0.081	0.011	0.100	0.100	0.100
MOLECULAR WEIGHT	LB/LBMOLE		20.311	20.311	20.311	18.029	18.029	18.029	18.029	18.029	18.029	18.029	73.048	73.048	73.048	73.048	73.048	73.048	72.857	72.857	72.857	72.857	72.857	72.857	72.857	72.857

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	EQUIPMENT LIS	T
ITEM	DESCRIPTION	MATERIAL
CL-7001	DISTILLATION COLUMN	316LSS/HASTELLOY C-276
F-700X	BOTTOMS FILTERS	316SS
HE-7001	FEED PREHEATER	SHELL: CARBON STEEL TUBES: 316LSS
HE-7002	STEAM HEATER	SHELL: CARBON STEEL TUBES: 316LSS
HE-7003	REBOILER	SHELL: CARBON STEEL TUBES: HASTELLOY C-276
HE-7004	PRODUCT COOLER	SHELL: CARBON STEEL TUBES: 316LSS
HE-7005	COLUMN CONDENSER	304SS/GASKETS EPDM
HE-7006	BOTTOM PURGE COOLER	SHELL: CARBON STEEL TUBES: HASTELLOY C-276
HE-7007	HEAT RECOVERY CONDENSER	304SS/GASKETS EPDM
PU-7002	BOTTOMS PUMP	HASTELLOY C
PU-7003	PRODUCT PUMP	316SS
PU-7004	REFLUX PUMP	316SS
TK-7002	REFLUX DRUM	316LSS

NOTES:

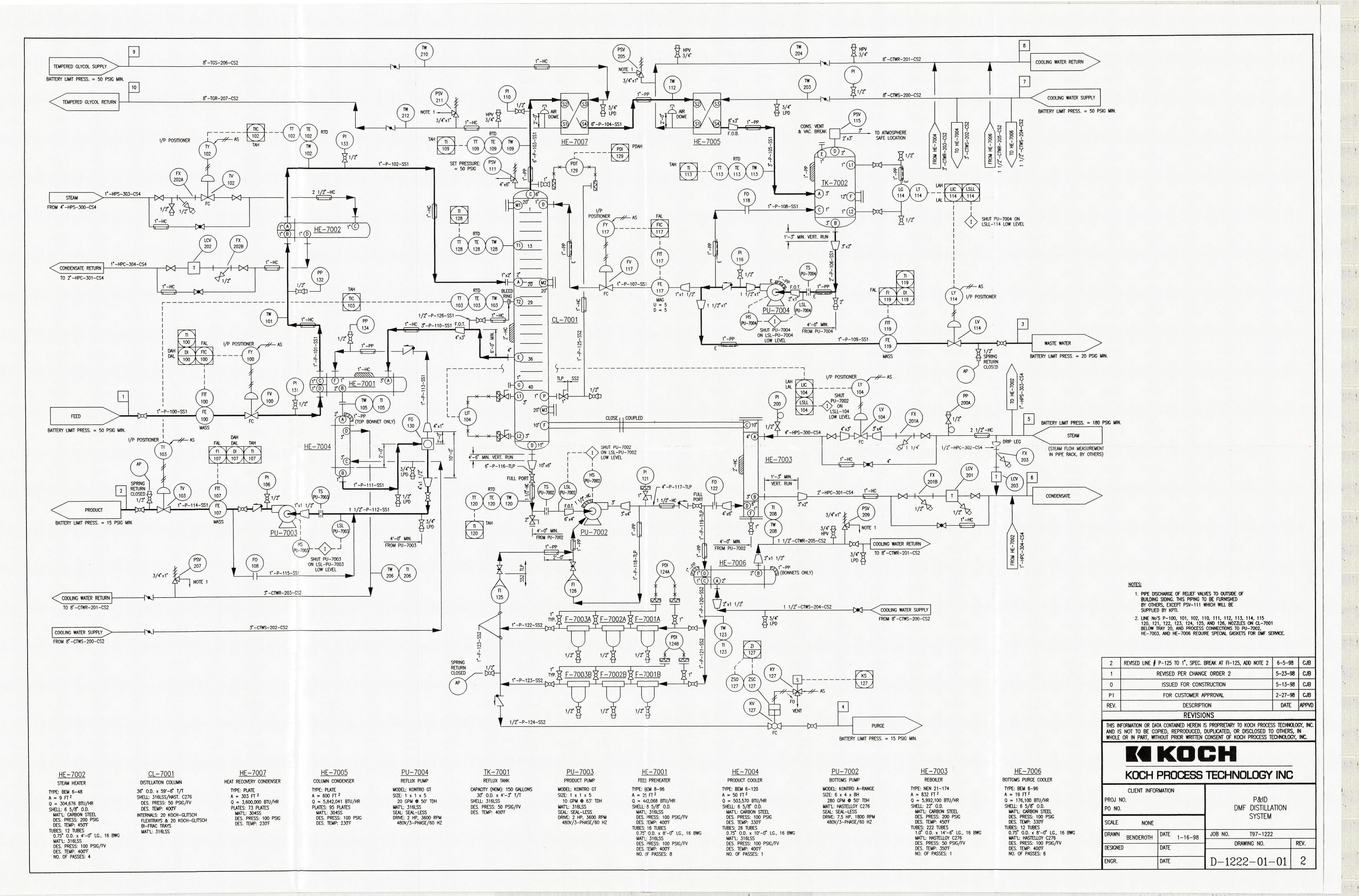
- 1. MATERIAL BALANCE SHOWN IS FOR 15% WT DMF AVERAGE FEED COMPOSITION.
- 2. UTILITIES DATA REFLECT MAXIMUM DUTY ACROSS THE 14-35% WT RANGE FOR THE DMF FEED.
- 3. WHEN HE-7007 IS NOT IN SERVICE STREAM 5 WILL BE AS STRRAM 4. 4. FOR MATERIAL BALANCE PURPOSE SOLIDS ARE CONSIDERED TO BE COMPLETELY REMOVED
- BY FILTERS.
- 5. NO ALLOWANCE IS MADE FOR SOLVENT LOSSES DUE TO CHANGING OF FILTERS.

PURGE

WATER

25 26 HOT MIN. FLOW BOTTOMS MAGNET FLUSH LIQUID TO PUMP RECYCLE PU-7002 0.0 0.0 1896.3 3410.7 25.5 45.9 19.4 19.4 3476.0 1941.2 328 234 26.5 9.0 54.171 51.546 0.249 0.396 4.7 8.0 0.575 0.546 0.081 0.089 72.857 72.857

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DMF Distillation Process Description

GENERAL PROCESS DESCRIPTION

The DMF Distillation System consists of a Distillation Column (CL-7001) with Koch-Glitsch valve trays, Feed Preheater (HE-7001), Steam Heater (HE-7002), Reboiler (HE-7003), Product Cooler (HE-7004), Column Condenser (HE-7005), Bottom Purge Cooler (HE-7006), Heat Recovery Condenser (HE-7007), Reflux Drum (TK-7002), Bottoms Pump (PU-7002), Product Pump (PU-7003) and Reflux Pump (PU-7004). Utilities consist of steam, cooling water, electricity and instrument air.

The feed containing DMF, water and formic acid is fed via Feed Preheater (HE-7001) and Steam Heater (HE-7002) to the Distillation Column (CL-7001) operating at atmospheric pressure. The column bottoms are circulated

by pump PU-7002, through Reboiler (HE-7003)

where 180 psig steam is used to generate vapors to strip water from the feed.

The formic acid in the feed forms a maximum boiling point azeotrope with the DMF and is rejected in a small purge stream from the

reboiler loop. Prior to leaving the unit this purge stream is cooled in the Bottoms Purge Cooler (HE-7006) to 115°F and filtered by

3-stage dual cartridge filters. Part of the filtered purge stream is recycled to the suction of pump PU-7002 as coolant for the magnets.

A vapor side draw is taken which contains the dry DMF product. The vapor product is condensed on the shell side of feed preheater (HE-7001) and then cooled to 115°F in Product Cooler (HE-7004) using 85°F cooling water.

The vapor from the stripping section, containing steam and a small quantity of DMF, is condensed in Column Condenser (HE-7005) and subcooled to 140°F. The condensate flows by gravity to the Reflux Drum from where it is pumped by PU-7004, either returning to the column as reflux or to battery limits of the system for disposal. When the Heat Recovery Condenser (HE-7007) is in service the vapors are first partially condensed in HE-7007 by 35%wt Propylene Glycol before passing to HE-7005 for remaining condensation and subcooling as before.

The DMF product contains less than 150 ppm wt water. The DMF concentration in the distillate product is less than 0.1% wt.

DESIGN CRITERIA

The expected performance of the system is based on computer simulations. The expected flow rates for the DMF distillation are presented below. Note that the content of formic acid in the products is based on the feed composition and does not include for decomposition of the DMF.

Wastewater Feed

DMF: 14-35 %wt Water: 64.8-84.9 %wt Formic Acid: 50 ppm Solids: 0.05-0.15 %wt Total (gpm): 8.0 Temperature (°F): 70 Pressure (psig): 20

Wastewater Distillate

Water: 99.9 %wt DMF: 0.1 %wt Flow rate (lb/h): 3373 Temperature (°F): 140 Pressure (psig): 20

DMF Product

Water: < 150 ppm wt DMF: > 99.96 % wt Formic Acid: < 400 ppm wt Flow rate (lb/h): 588.4 Temperature (°F): 115 Pressure (psig): 15

Bottoms Purge Stream

DMF: 98.8 %wt Formic Acid: 1.2 %wt Solids: < 5.0 %wt Flow rate (lb/h): 3.2 Temperature (°F): 115 Pressure (psig): 5.0

Utilities

Steam: 7419 lb/hr @ 180 psig (saturated)
Cooling Water: 915 GPM @ 60 psig and 85°F, 15°F temperature rise
Electricity: 480V, 3 phase, 6.2 kW (11.5 H.P. total connected)
Instrument Air: Approximately 75 SCFH, @ 100 psig, -40°F dew point, oil and water free